

# Flexible Control of Nuclear Cogeneration Plants for Balancing Intermittent Renewables

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**Abstract:** Due to the complementarity between the intermittent renewable energy (IRE) and the nuclear, it is attractive to interconnect them to supply clean energy consistently and continuously in a large-scale. The flexibility of for integrating the IRE can be provided by actively adjusting the electric power output of nuclear cogeneration plants (NCPs), which induces frequent redistribution of main steam to the turbine and cogeneration process. For the main steam redistribution, it is necessary to guarantee the stability of grid frequency and main steam pressure, which heavily relies on the flexible control of NCPs. In this paper, a new flexible control of NCPs with saturated main steam is proposed based upon the idea of actively suppressing the total disturbance in the dynamics of grid frequency and that of main steam pressure. The stabilization problems of pressure and frequency are transferred to the disturbance attenuation problem of a second-order system, and an active disturbance rejection control (ADRC) is then proposed. This ADRC is applied to the flexible control of a NCP composed of a nuclear heating reactor (NHR), a turbine-generator set and a multi-effect-desalination and thermal-vapor-compression (MED-TVC) process for seawater desalination. Numerical simulation results in the cases of load stepping show that the flexibility of this NCP is satisfactory in balancing the grid.

*Keywords:* renewable integration, nuclear cogeneration, disturbance attenuation

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## 1. INTRODUCTION

Although intermittent renewable energy (IRE) resources such as the wind and solar are going to make our planet a better place to live (Alizadeh, et al., 2016), however since IRE cannot provide power supply consistently and continuously, the large-scale integration of IRE may significantly aggravate the grid imbalance (Lund, et al., 2015). Actually, the integration cost has been a key part in the total cost of IRE generation [3]. With comparison to IRE, nuclear power plants (NPPs) are able to provide consistent and clean power supply with small land footprint (Kondziella and Bruckner, 2016). Nuclear power practices have been adapted over the years for balancing power supply and demand either due to the high share of nuclear in the energy mix such as France or the massive deployment of IRE in the mix such as Germany (Suman, 2018).

The flexibility of nuclear plants for grid balance can be given by either load-following or cogeneration. To provide satisfactory level of flexibility while keeping a higher load factor of nuclear reactors, cogeneration is better to be used, where the frequency fluctuation caused by IRE generation is stabilized by bypassing the excess main steam flow provided by a nuclear steam supplying system (NSSS) to the backup cogeneration processes for desalination, hydrogen production, natural gas reforming and etc. (Locatelli, et al., 2017). With comparison to the nuclear plants providing flexibility through load-

following, the reactor of a nuclear cogeneration plant (NCP) is kept at a constant level, where the redistribution of main steam is given by the electric power from IRE plants (Cany, et al., 2016). Although there have already been abundant results for the load-following control of nuclear power plants (Li, et al, 2016), there is still very limited results in the flexible control of NCPs

In this paper, the flexible control of NCP is realized by stabilizing the grid frequency and main steam pressure based upon the redistribution of main steam. An active disturbance rejection control (ADRC) is proposed for the stabilization, which contains a proportional-integral feedback term and a feedforward term driven by a 3<sup>rd</sup>-order disturbance observer (DO). Then, this ADRC is applied for the flexible control of a NCP based on nuclear heating reactor for electricity generation and seawater desalination. Simulation results in the case of power stepping show that this NCP flexible controller is feasible for the grid balance in the context of deep renewable penetration.

## 2. MODELING AND PROBLEM FORMULATION

The control design oriented state-space models of the dynamics of main steam pressure and that of grid frequency are given, and the control problem is formulated.

### 2.1 State-Space model of Main Steam Pressure Error

Based on the energy conservation law, the energy balance for the secondary side of steam generators can be given by

$$V_s \frac{d}{dt} (\rho_s h_s) = Q_{in} + G_{fw} h_{fw} - (G_{tb} + G_{co}) h_{st}, \quad (1)$$

where  $V_s$  is the total volume of the secondary sides of steam generators (SGs),  $\rho_s$  and  $h_s$  are respectively the average density and enthalpy of secondary coolant of steam generator (SG),  $Q_{in}$  is the heat flux from the primary to the secondary sides of SG,  $G_{fw}$  and  $h_{fw}$  are respectively the mass flowrate and enthalpy of SG feedwater,  $G_{tb}$  and  $G_{co}$  are the steam flowrates at the inlet of turbine and cogeneration process respectively, and  $h_{st}$  is the enthalpy of main steam. It is assumed that both

$$\rho_s h_s = (\rho_{fw} h_{fw} + \rho_{st} h_{st}) / 2, \quad (2)$$

and the product  $\rho_{fw} h_{fw}$  are constant, where  $\rho_{fw}$  is the density of SG feedwater, and  $\rho_{st}$  and  $h_{st}$  are respectively the density and enthalpy of main steam. Based on this assumption, energy balance equation (1) can be rewritten as

$$\frac{V_s}{2} \frac{d}{dt} (\rho_{st} h_{st}) = Q_{in} + W_{fw} (\rho_{fw} h_{fw}) - (G_{tb} + G_{co}) h_{st}, \quad (3)$$

where  $W_{fw} = G_{fw} / \rho_{fw}$  is volume flowrate of SG feedwater. Here, steam flows  $G_{tb}$  and  $G_{co}$  can be represented as

$$G_a = C_a X_a \sqrt{\rho_{st} P_{st}}, \quad (4)$$

where footnote a=tb, co representing turbine-generator system and cogeneration process respectively,

$$X_a = \sqrt{1 - P_a / P_{st}}, \quad (5)$$

$C_a$  is the conductance of flowrate control actuator such as the steam regulating valve of turbine and the ejector of MED-TVC process,  $P_{st}$  is the main steam pressure, and  $P_a$  is the pressure just after the actuator. For the turbine-generator system, since the difference between  $P_{st}$  and  $P_{tb}$  is small so as to keep the efficiency,  $X_{tb}$  is very small. For the MED-TVC process, since the pressure at the ejector throat is much lower than  $P_{st}$ , it can be seen that  $X_{co} \approx 1$ . Thus, it is reasonable to assume that scalar  $X_a$  (a=tb, co) are positive constants.

Furthermore, based upon the fact that the main steam is saturated as well as the assumptions that both product  $\rho_{fw} h_{fw}$  and scalar  $X_a$  are constant, the error dynamics of main steam pressure can be derived from equation (3) as

$$\begin{aligned} \frac{V_s}{2} \left[ \frac{\partial (\rho_{st} h_{st})}{\partial P_{st}} \right]_{P_{st0}} \frac{d\Delta P_{st}}{dt} = \Delta Q_{in} + \Delta W_{fw} (\rho_{fw} h_{fw}) - \\ (X_{tb} C_{tb0} + X_{co} C_{co0}) \left[ \frac{\partial (h_{st} \sqrt{\rho_{st} P_{st}})}{\partial P_{st}} \right]_{P_{st0}} \Delta P_{st} - \\ h_{st0} \sqrt{\rho_{st0} P_{st0}} (X_{tb} \Delta C_{tb} + X_{co} \Delta C_{co}), \quad (6) \end{aligned}$$

where  $\Delta P_{st} = P_{st} - P_{st0}$ ,  $\Delta W_{fw} = W_{fw} - W_{fw0}$ ,  $\Delta Q_{in} = Q_{in} - Q_{in0}$ ,  $\Delta C_{tb} = C_{tb} - C_{tb0}$  and  $\Delta C_{co} = C_{co} - C_{co0}$ , and  $P_{st0}$ ,  $W_{fw0}$ ,  $Q_{in0}$ ,  $C_{tb0}$  and  $C_{co0}$  are the expected steady values of  $P_{st}$ ,  $W_{fw}$ ,  $Q_{in}$ ,  $C_{tb}$  and  $C_{co}$  at a given power-level,  $\rho_{st0}$  and  $h_{st0}$  are the steady values of  $\rho_{st}$  and  $h_{st}$ . Since the steam is saturated,  $\rho_{st0}$  and  $h_{st0}$  are given by  $P_{st0}$ .

Choose the state-vector  $x$  and control input  $u$  respectively as

$$x = [x_1 \quad x_2]^T = \left[ \int_0^t \Delta P_{st}(\tau) d\tau \quad \Delta P_{st}(t) \right]^T, \quad (7)$$

$$u = -\Delta C_{co}. \quad (8)$$

Then, steam pressure error dynamics (6) can be rewritten as the following state-space model

$$\begin{cases} \dot{x}_1 = x_2, \\ \dot{x}_2 = -ax_2 + bu + d, \end{cases} \quad (9)$$

by choosing

$$a = \left\{ \frac{V_s}{2} \left[ \frac{\partial (\rho_{st} h_{st})}{\partial P_{st}} \right]_{P_{st0}} \right\}^{-1} (X_{tb} C_{tb0} + X_{co} C_{co0}) \left[ \frac{\partial (h_{st} \sqrt{\rho_{st} P_{st}})}{\partial P_{st}} \right]_{P_{st0}}, \quad (10)$$

$$b = \left\{ \frac{V_s}{2} \left[ \frac{\partial (\rho_{st} h_{st})}{\partial P_{st}} \right]_{P_{st0}} \right\}^{-1} X_{co} h_{st0} \sqrt{\rho_{st0} P_{st0}}, \quad (11)$$

$$d = \left\{ \frac{V_s}{2} \left[ \frac{\partial (\rho_{st} h_{st})}{\partial P_{st}} \right]_{P_{st0}} \right\}^{-1} \left[ \Delta Q_{in} + \Delta W_{fw} (\rho_{fw} h_{fw}) - X_{tb} h_{st0} \sqrt{\rho_{st0} P_{st0}} \Delta C_{tb} \right], \quad (12)$$

from which it can be seen that  $a$  and  $b$  are constants, and  $d$  is bounded and varied with the operational condition.

## 2.2 State-Space Model of Grid Frequency

The swing equation of a synchronous generator governing the grid frequency and rotor angle can be expressed as

$$\begin{cases} \dot{\delta} = \omega - 1, \\ \dot{\omega} = \frac{P_m}{\omega H} - T_e, \end{cases} \quad (13)$$

where  $\delta$  is the rotor angle in the synchronously rotating frame,  $\omega$  is the normalized rotation-rate,  $H$  is the mechanical inertia of rotor,  $P_m$  is the mechanical power given by the turbine,  $T_e$  the electromagnetic torque given by the grid. For a classical multi-machine grid, electromagnetic torque  $T_e$  satisfies

$$T_e = GE_q'^2 + E_q' \sum_{k=1}^n \omega_k E_{q,k}' (G_k \cos \delta_k + B_k \sin \delta_k) \quad (14)$$

where  $E_q'$  and  $G$  are the voltage and self-conductance of the local generator,  $\delta_k$  is the rotor angle of the  $k$ th remote generator in the local rotating frame, and  $\omega_k$ ,  $E_{q,k}'$ ,  $G_k$  and  $B_k$  are the rotation-rate, transient voltage, conductance and susceptance of the  $k$ th remote generator respectively.

From swing equation (13), the error dynamics of rotor angle and rotation-rate can be given by

$$\begin{cases} \Delta \dot{\delta} = \Delta \omega, \\ \Delta \dot{\omega} = -\frac{P_m}{\omega H} \Delta \omega + \frac{\Delta P_m}{H} - \Delta T_e, \end{cases} \quad (15)$$

where  $\Delta \delta = \delta - \delta_0$ ,  $\Delta \omega = \omega - \omega_0$ ,  $\Delta P_m = P_m - P_{m0}$ ,  $\Delta T_e = T_e - T_{e0}$ , and  $\delta_0$ ,  $\omega_0$ ,  $P_{m0}$  and  $T_{e0}$  are respectively the setpoints of  $\delta$ ,  $\omega$ ,  $P_m$  and  $T_e$  with  $\omega_0 = 1$  and  $P_{m0} = HT_{e0}$ .  $\Delta P_m$  can be expressed as

$$\Delta P_m = \frac{\Delta G_{tb}}{G_{tbr}} + d_m, \quad (16)$$

where constant  $G_{tbr}$  is the steam flowrate to the turbine at the rated electrical power-level,  $\Delta G_{tb} = G_{tb} - G_{tb0}$ ,  $G_{tb0}$  is the referenced value of  $G_{tb}$ , and  $d_m$  is a scalar. Based on equation (4),

$$\Delta P_m = \frac{\sqrt{\rho_{st0} P_{st0}} X_{tb}}{G_{tbr}} \Delta C_{tb} + \frac{X_{tb} C_{tb0}}{G_{tbr}} \left[ \frac{\partial \left( \sqrt{\rho_{st} P_{st}} \right)}{\partial P_{st}} \right]_{P_{st0}} \Delta P_{st} + d_m. \quad (17)$$

Substitute equations (17) to (15),

$$\begin{cases} \Delta \dot{\delta} = \Delta \omega, \\ \Delta \dot{\omega} = -\frac{P_m}{H\omega} \Delta \omega + \frac{\sqrt{\rho_{st0} P_{st0}} X_{tb}}{HG_{tbr}} \Delta C_{tb} + \\ \frac{X_{tb} C_{tb0}}{HG_{tbr}} \left[ \frac{\partial \left( \sqrt{\rho_{st} P_{st}} \right)}{\partial P_{st}} \right]_{P_{st0}} \Delta P_{st} + \frac{d_m}{H} - \Delta T_e. \end{cases} \quad (18)$$

By choosing the state-vector  $\mathbf{x}$  and control input  $u$  as

$$\mathbf{x} = [x_1 \quad x_2]^T = [\Delta \delta \quad \Delta \omega]^T, \quad (19)$$

$$u = \Delta C_{tb}, \quad (20)$$

error dynamics (18) can be also represented as state-space model (9) with constants  $a$  and  $b$  as well as total disturbance  $d$  defined respectively as

$$a = \frac{P_{m0}}{H}, \quad (21)$$

$$b = \frac{\sqrt{\rho_{st0} P_{st0}} X_{tb}}{HG_{tbr}}, \quad (22)$$

$$d = \frac{\omega P_{m0} - P_m}{H\omega} \Delta \omega + \frac{X_{tb} C_{tb0}}{HG_{tbr}} \left[ \frac{\partial \left( \sqrt{\rho_{st} P_{st}} \right)}{\partial P_{st}} \right]_{P_{st0}} \Delta P_{st} + \frac{d_m}{H} - \Delta T_e. \quad (23)$$

### 2.3 Control Problem Formulation

From state-space model (9), the stabilization problem of both the main steam pressure and grid frequency can be converted to the theoretical control problem summarized as follows.

**Problem.** Consider the 2<sup>nd</sup> order dynamical system

$$\dot{\mathbf{x}} = \mathbf{A}\mathbf{x} + \mathbf{b}u + \mathbf{d} \quad (24)$$

where  $\mathbf{x}=[x_1 \quad x_2]^T$  is the state-vector,  $u$  is control input,

$$\mathbf{A} = \begin{bmatrix} 0 & 1 \\ 0 & -a \end{bmatrix}, \quad (25)$$

$$\mathbf{b} = [0 \quad b]^T, \quad (26)$$

$$\mathbf{d} = [0 \quad d]^T, \quad (27)$$

both  $a$  and  $b$  are given positive constants, and  $d$  is called total disturbance satisfying

$$\dot{d} = D, \quad (28)$$

where

$$|D| \leq M_d, \quad (29)$$

and  $M_d$  is a bounded positive constant. How to design control input  $u$  so that  $\mathbf{x} \rightarrow \mathcal{E}$  as  $t \rightarrow \infty$ , where  $\mathbf{x}=[x_1, x_2]^T$  is the state-vector and  $\mathcal{E} \subset \mathbb{R}^2$  is a bounded set including the origin  $\mathbf{x}=\mathbf{0}$ .

## 3. FLEXIBLE CONTROL BASED ON ACTIVE DISTURBANCE ATTENUATION

From system model (24), it is can be seen that the central in guaranteeing the closed-loop stability is to effectively attenuate total disturbance  $d$ . However, from (12) and (23), disturb-

ance  $d$  is influenced by many uncertain variables and is impossible to be known accurately, which extensively increase the difficulty in solving the control problem. In this section, instead of modelling the total disturbance, a disturbance observer is given based upon the measurements of system state-vector, and an active disturbance rejection control (ADRC) is then proposed for globally bounded stabilization. This result is summarized as the following theorem.

**Theorem.** Consider system (24) with state variables measurable. Suppose that total disturbance  $d$  satisfies (28) and (29) with positive constant  $M_d$  being bounded. Then, ADRC

$$u = -b^{-1} (k_2 x_1 + k_1 x_2) - b^{-1} \hat{d}, \quad (30)$$

where  $k_i > 0$  ( $i=1, 2$ ) is the feedback gains, and  $\hat{d}$  is the estimation of total disturbance  $d$  given by 3<sup>rd</sup>-order disturbance observer (DO)

$$\begin{cases} \dot{\hat{x}}_1 = \hat{x}_2 - \gamma_1 \varepsilon^{-1} e_1 \\ \dot{\hat{x}}_2 = -a \hat{x}_2 + bu + \hat{d} - \gamma_2 \varepsilon^{-2} e_1, \\ \dot{\hat{d}} = -\gamma_3 \varepsilon^{-3} e_1, \end{cases} \quad (31)$$

with  $\gamma_i > 0$  is the observer gains ( $i=1, 2, 3$ ), constant  $\varepsilon \in (0, 1)$ ,

$$e_i = \hat{x}_i - x_i, \quad i=1, 2, \quad (32)$$

ADRC (30) can provide globally bounded closed-loop stability if all the roots of algebraic equations

$$s^3 + (\gamma_1 + \varepsilon a)s^2 + (\gamma_2 + \varepsilon a \gamma_1)s + \gamma_3 = 0, \quad (33)$$

and

$$s^2 + (k_1 + a)s + k_2 = 0, \quad (34)$$

have negative real parts.

**Proof.** First, the convergence of DO (31) is analysed. Define the estimation error of total disturbance  $d$  as

$$e_3 = \hat{d} - d. \quad (35)$$

Then, from (24), (29) and (31), the observation errors  $e_i$  ( $i=1, 2, 3$ ) satisfy dynamical equation

$$\begin{cases} \dot{e}_1 = -\gamma_1 \varepsilon^{-1} e_1 + e_2 \\ \dot{e}_2 = -\gamma_2 \varepsilon^{-2} e_1 - a e_2 + e_3, \\ \dot{e}_3 = -\gamma_3 \varepsilon^{-3} e_1 - D. \end{cases} \quad (36)$$

Based on coordination transformation

$$\mathbf{z} = [z_1 \quad z_2 \quad z_3]^T = [e_1 \quad \varepsilon e_2 \quad \varepsilon^2 e_3]^T \quad (37)$$

and scale transformation

$$\tau = \varepsilon^{-1} t, \quad (38)$$

estimation error dynamics (36) can be rewritten as

$$\frac{d\mathbf{z}}{d\tau} = \mathbf{A}_0 \mathbf{z} - \varepsilon^3 \mathbf{D}, \quad (39)$$

where

$$\mathbf{A}_0 = \begin{bmatrix} -\gamma_1 & 1 & 0 \\ -\gamma_2 & -\varepsilon a & 1 \\ -\gamma_3 & 0 & 0 \end{bmatrix}, \quad (40)$$

$$\mathbf{D} = [0 \quad 0 \quad D]^T. \quad (41)$$

As  $\varepsilon$  is strictly positive, the stability of error dynamics (36) is equivalent to system (39). Moreover, due to (33) is the characteristic equation of matrix (40), and due to all the roots of (33) have strict negative real parts, for an arbitrarily given

positive-definite symmetric matrix  $\mathbf{Q}_0$ , there exists a positive-definite  $\mathbf{P}_0$  so that Lyapunov equation

$$\mathbf{A}_0^T \mathbf{P}_0 + \mathbf{P}_0 \mathbf{A}_0 = -\mathbf{Q}_0. \quad (42)$$

is well satisfied.

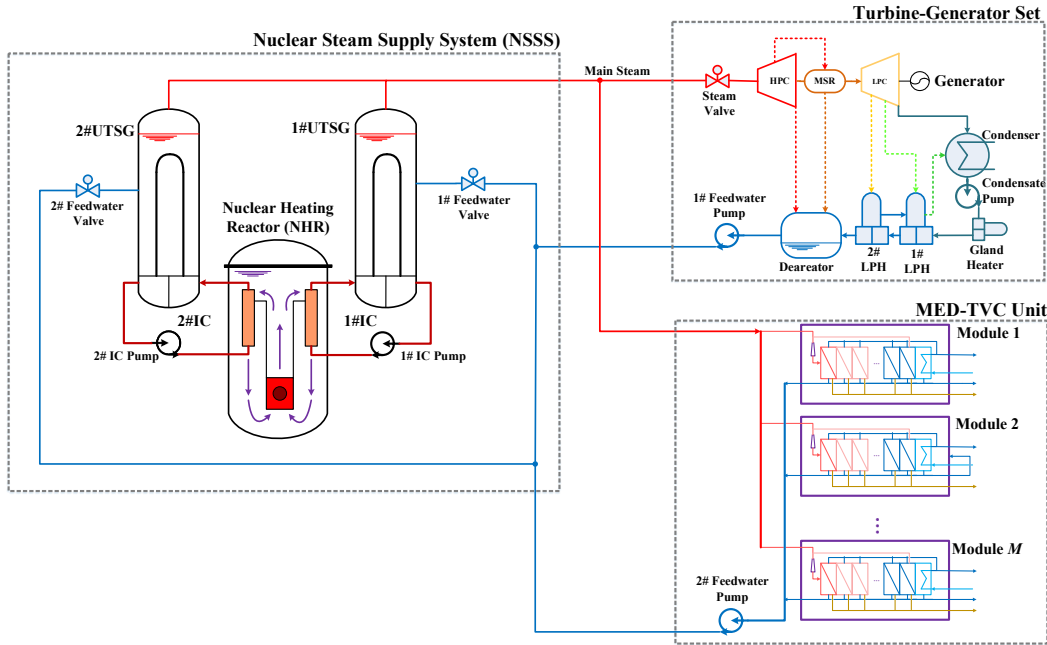


Fig.1. Schematic process diagram of a nuclear heating reactor electricity-water cogeneration plant

From (42), choose the Lyapunov function for system (39) as

$$V_0(z) = z^T \mathbf{P}_0 z, \quad (43)$$

and differentiate  $V_0$  along the trajectory of system (39),

$$\begin{aligned} \frac{dV_0(z)}{d\tau} &= 2z^T \mathbf{P}_0 (\mathbf{A}_0 z - \varepsilon^3 \mathbf{D}) \\ &= z^T (\mathbf{P}_0 \mathbf{A}_0 + \mathbf{A}_0^T \mathbf{P}_0) z - 2\varepsilon^3 z^T \mathbf{P}_0 \mathbf{D} \\ &\leq -\frac{1}{2} z^T \mathbf{Q}_0 z + 2\varepsilon^6 \mathbf{D}^T \mathbf{P}_0 \mathbf{Q}_0^{-1} \mathbf{P}_0 \mathbf{D}. \end{aligned} \quad (44)$$

From inequality (44), vector  $z$  converges globally and asymptotically to a bounded set around the origin, which means that DO (31) provides a globally bounded estimation of total disturbance  $d$ . It can be also seen that if constant  $\varepsilon$  is smaller and the real parts of the roots of (34) are more negative, then the bounded set around the origin is tighter.

Second, the stability of closed-loop system constituted by (24), (30) and (31) is analyzed. From equation (24) and (30), the closed-loop dynamics can be written as

$$\dot{\mathbf{x}} = \mathbf{A}_c \mathbf{x} - \mathbf{E}_d, \quad (45)$$

where

$$\mathbf{A}_c = \begin{bmatrix} 0 & 1 \\ -k_2 & -(k_1 + a) \end{bmatrix}, \quad (46)$$

$$\mathbf{E}_d = [0 \quad e_3]^T. \quad (47)$$

Since gains  $k_1$  and  $k_2$  are chosen so that both the two roots of algebraic equation (34) have strict real parts, for an arbitrarily given positive-definite symmetric matrix  $\mathbf{Q}_c$ , there exists a positive-definite matrix  $\mathbf{P}_c$  satisfying Lyapunov equation

$$\mathbf{A}_c^T \mathbf{P}_c + \mathbf{P}_c \mathbf{A}_c = -\mathbf{Q}_c. \quad (48)$$

Then, choose Lyapunov function of system (45) as

$$V_c(\mathbf{x}) = \mathbf{x}^T \mathbf{P}_c \mathbf{x}, \quad (49)$$

and differentiate function  $V_c$  along the trajectory of (45),

$$\begin{aligned} \dot{V}_c(\mathbf{x}) &= 2\mathbf{x}^T \mathbf{P}_c (\mathbf{A}_c \mathbf{x} - \mathbf{E}_d) \\ &= \mathbf{x}^T (\mathbf{A}_c^T \mathbf{P}_c + \mathbf{P}_c \mathbf{A}_c) \mathbf{x} - 2\mathbf{x}^T \mathbf{P}_c \mathbf{E}_d \\ &\leq -\frac{1}{2} \mathbf{x}^T \mathbf{Q}_c \mathbf{x} + 2(\boldsymbol{\eta}^T \mathbf{P}_c \mathbf{Q}_c^{-1} \mathbf{P}_c \boldsymbol{\eta}) e_3^2, \end{aligned} \quad (50)$$

where  $\boldsymbol{\eta} = [0 \quad 1]^T$ .

From the performance analysis of DO (31), disturbance estimation error  $e_3$  can be arbitrarily small by properly choosing  $\varepsilon$ . Hence, from inequality (50), state  $\mathbf{x}$  converges globally and asymptotically to a bounded set around the origin. The proof is completed.

**Remark.** From system model (24), it can be seen that ADRC (30) can be rewritten as

$$u = -\frac{1}{b} \left[ k_1 x_2 + k_2 \int_0^t x_2(\tau) d\tau \right] - \frac{\hat{d}}{b}, \quad (51)$$

which is an addition of a proportional-integral (PI) feedback action and a feedforward action driven by DO (31).

## 4. APPLICATION TO A NHR COGENERATION PLANT

### 4.1 The NHR Cogeneration plant and its Control System

The schematic process diagram of the nuclear heating reactor (NHR) plant cogenerating electricity and desalinated water is shown in Fig. 1. This NCP is mainly composed of a NSSS, a turbine-generator set and a MED-TVC desalination process, where the NSSS is further composed of a 200MW<sub>t</sub> NHR, two forced-circulated intermediate circuits (ICs) and two U-tube steam generators (UTSGs) giving saturated live steam (Dong, Pan, 2018). The heat is transferred from the reactor to steam generators via two ICs, and converts the feedwater to saturat-

ed live steam. The live steam flows from the two UTSGs are combined to form the main steam flow which is then distrib-

uted to both the turbine and MED-TVC modules for electricity generation and seawater desalination.

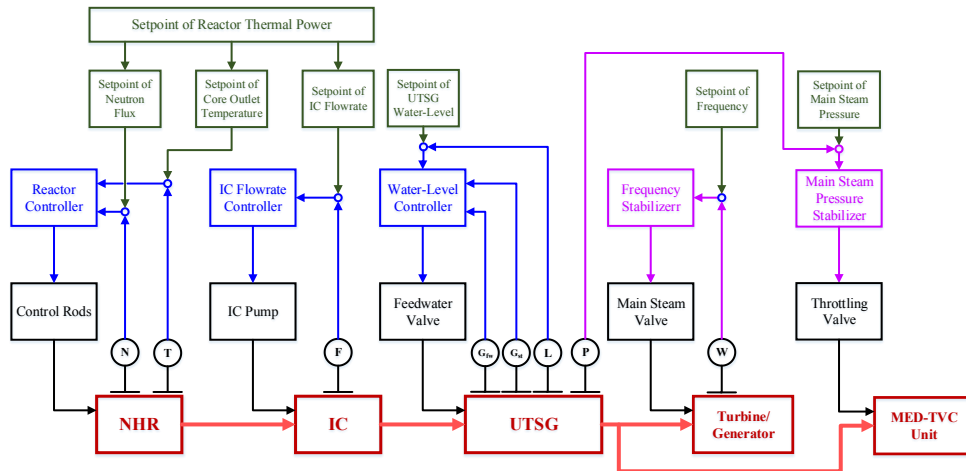


Fig. 2. Flexible control scheme of NHR cogeneration plant

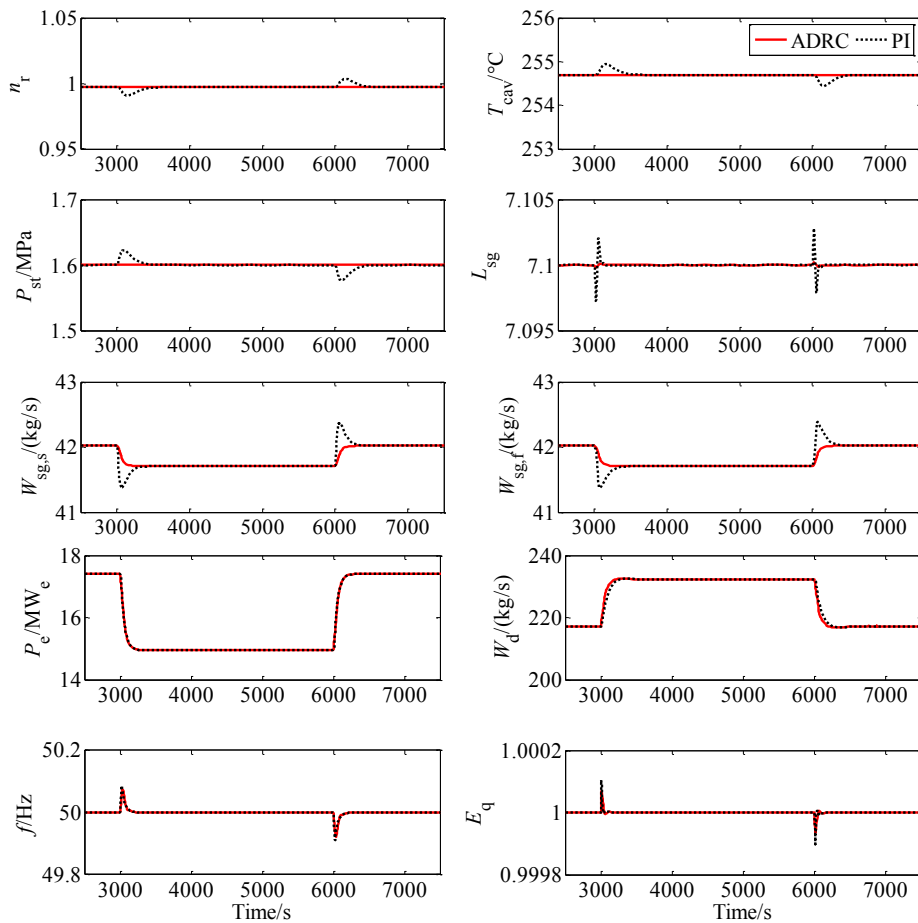


Fig. 3. Simulation results in the case of load stepping,  $n_r$ : neutron flux,  $T_{cav}$ : average temperature of primary coolant,  $P_{st}$ : main steam pressure,  $L_{sg}$ : UTSG water-level,  $W_{sgs}$ : main steam flowrate,  $W_{sgf}$ : feedwater flowrate,  $P_e$ : electric power,  $W_d$ : product of potable water,  $f$ : grid frequency, and  $E_q$ : normalized voltage.

The coordinated control system of NHR cogeneration plant is schematically illustrated in Fig. 2. The NSSS control system is constituted by the reactor controller, IC flowrate controller and water-level controller, which generates the driving signal of control rods, IC pumps and feedwater valves based on the setpoints and measurements of neutron flux, core outlet temperature, IC flowrates and UTSG water-levels. The regulation algorithms of NSSS control systems adopts the classical pro-

portional-differential-integral (PID) feedback laws presented in (Dong, 2013; Dong, et al. 2009). The flexible control system is formed by the frequency stabilizer and the main steam pressure stabilizer which adopt the ADRC given in Section 3 as control algorithm to generate the expected opening of the main steam valve of turbine and the expected ejector nozzle cross-section area of every MED-TVC module.

#### 4.2 Simulation Result

To show the feasibility of ADRC (30) in the flexible control of NHR cogeneration plant, numerical simulation is done on Matlab/Simulink platform. In the simulation, the performance of ADRC (30) is compared with that of the PI control given by equation (51) without the last term driven by the disturbance estimation are compared with each other. The case considered in this simulation is load stepping: Initially, the NHR operates at its rated power, where 70% of main steam flow are used for electricity generation. At 3000s, a load in the grid steps down with an amplitude of 2.5MW<sub>e</sub>, and the load steps back up to its original level at 6000s. The transient responses of some key process variables are shown in Fig. 3.

#### 4.3 Discussions

From Fig. 3, when the electric load steps down, the grid frequency increases quickly, which drives the frequency stabilizer to decrease the opening of main steam regulating valve at the inlet of turbine so as to maintain power balance. As the electric power balance is reached, the frequency returns to its setpoint. The smaller opening of turbine steam valve leads to the increase of steam pressure, which is further suppressed by the main steam pressure stabilizer via enlarging the cross-section area of ejector nozzles in MED-TVC modules.

From Fig. 3, though both the ADRC and PI control can keep the balance of power and heat, the difference between the two control strategies in the aspect of control performance is apparent. The overshoots of neutron flux, primary coolant temperature, main steam pressure and UTSG water-level induced by the ADRC is much smaller than those induced by the classical PI controller. The overshoot of grid frequency during load stepping given by the ADRC is smaller than that given by the PI controller. Moreover, since the overshoot of terminal voltage corresponding to the ADRC is smaller than that corresponding to the PI in both the cases of load stepping and ramping, it can be seen that ADRC can induce a slower frequency variation rate. Actually, the difference in the control performance is induced by the feedforward term, i.e. the last term in (51) given by the total disturbance estimation from DO (31). The total disturbance  $d$  can induce a stronger deviation in the process variables if there is no feedforward term attenuating the disturbance actively. The effectiveness of DO (31) is manifested by the higher performance of ADRC which relies on the convergence of disturbance estimation.

In a summary, with comparison to the classical PI algorithm, the ADRC (51) can keep a better balance between the supply and consumption of power and heat. Moreover, since DO (31) can easily realized by a program on any digital control system platforms, ADRC (51) is practically implementable.

### 5. CONCLUSIONS

To suppress the grid fluctuation caused by the IRE generation, it is necessary to study the flexible control of NCPs, whose central problem is to redistribute the main steam between the turbine and cogeneration process according to IRE

generation. In this paper, a flexible control strategy of NCPs with saturated main steam is newly proposed based upon the idea of active disturbance attenuation. The flexibility is realized by the stabilization of grid frequency and main steam pressure through main steam flow redistribution, where the stabilization is further transferred to the disturbance attenuation of a 2<sup>nd</sup>-order dynamical system. Then, an ADRC is originally designed for realizing disturbance attenuation, where the disturbance estimation is provided by a novel 3<sup>rd</sup>-order DO. Finally, this newly-built ADRC is applied to the flexible control of a NCP composed of a NHR, a turbine-generator set and a MED-TVC seawater desalination process, and numerical simulation results show that the flexibility of this NCP is satisfactorily guaranteed by the flexible control strategy for grid balancing.

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